

FLOW OF A MIXTURE OF RAREFIED GASES BETWEEN
TWO PARALLEL PLATES WITH SINUSOIDAL
CONCENTRATION DISTRIBUTION AT
THE BOUNDARY

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UDC 533.5

We investigate the effect of the transverse velocity component at a gas-plate boundary on the flow regime of a two-component rarefied gas between two parallel plates with sinusoidal concentration distribution on the lower plate.

We consider the isothermal flow of a two-component rarefied gas between two parallel plates with a sinusoidal concentration distribution on the lower plate.

We choose the X and Y axes, respectively, along, and along the normal to the surface of the lower plate. The concentration on the upper plate (Y = d) is constant and equals c_d , and on the lower plate the concentration is of the form

$$c = c_0 \left(1 + \alpha \sin \frac{2\pi X}{L} \right).$$

We assume the following quantities to be small: the ratio $(c_0 - c_d)/c_0$, the coefficient α , and the ratio of the mean free path of gas molecules to the wavelength L of the concentration variation. For $c_0 \neq c_d$ and $\alpha = 0$, there is a transverse motion of gas between the plates. For $\alpha \neq 0$ on the lower plate there is diffusion slip, as a result of which there arises slow macroscopic motion (the velocities u and v are small).

We seek the pressure, density, and concentration distributions in the form

$$p = p_0(1 + \xi), \quad \rho = \rho_0(1 + \sigma), \quad c = c_0(1 + \tau).$$

The quantities with subscripts zero correspond to the undisturbed lower plate ($\alpha = 0$, $c = c_0$), ξ , σ , and τ are small.

Disregarding products of small quantities, we write the system of equations [1]

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$\frac{\partial \xi}{\partial x} = \mu_* \Delta u, \tag{2}$$

$$\frac{\partial \xi}{\partial y} = \mu_* \Delta v, \tag{3}$$

$$\Delta \tau = 0, \tag{4}$$

$$\xi = \sigma + m\tau. \tag{5}$$

Here we have introduced the following notation:

$$x = \frac{2\pi X}{L}, \quad y = \frac{2\pi Y}{L}, \quad \mu_* = \frac{2\pi \mu}{\rho_0 L},$$

$$m = 1 - \frac{\rho_0 R_2 T}{\rho_0}.$$

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Translated from *Inzhenerno-Fizicheskii Zhurnal*, Vol. 17, No. 5, pp. 958-961, November, 1969. Original article submitted December 9, 1968.

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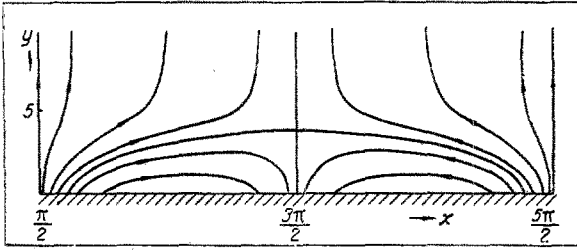


Fig. 1. Streamlines corresponding to the stream function (22).

We now state the boundary conditions. On the lower plate we must use a condition that takes account of diffusion slip [2, 3]. Furthermore, we consider the nonzero transverse velocity component at the gas-wall boundary [4].

Accordingly, the boundary conditions (in the same approximation as for the equation) are of the following form:

for $y = 0$

$$a_1 \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) + a_2 \frac{\partial \tau}{\partial x} + a_3 u = 0, \quad (6)$$

$$-v(1 - c_0) = a_4 \frac{\partial \tau}{\partial y}, \quad (7)$$

$$\tau = \alpha \sin x, \quad (8)$$

where

$$a_1 = -\frac{(2-f)\pi\mu}{fL},$$

$$a_2 = -\frac{2\pi\rho_0 D_{12}c_0}{L} \left(\frac{T}{2\pi} \right)^{1/2} (R_1^{1/2} - R_2^{1/2}), \quad (9)$$

$$a_3 = \rho_0 \left(\frac{T}{2\pi} \right)^{1/2} [c_0 R_1^{1/2} + (1 - c_0) R_2^{1/2}],$$

$$a_4 = \frac{2\pi D_{12}c_0}{L};$$

for $y = 2\pi d/L$, we use a condition similar to (6), and also the conditions

$$-v(1 - c_d) = a_4 \frac{\partial \tau}{\partial y}, \quad (10)$$

$$\tau = \frac{c_d - c_0}{c_0}. \quad (11)$$

Solving Eq. (4) with conditions (8) and (11) (assuming the quantity $\exp\{-2\pi d/L\}$ to be negligible), we obtain

$$\tau = \alpha \exp\{-y\} \sin x + \frac{L(c_d - c_0)}{2\pi d c_0} y. \quad (12)$$

Eliminating u and v from (1)-(3), we obtain the equation

$$\Delta \xi = 0, \quad (13)$$

which has the solution

$$\xi = 2\mu_* b_1 \exp\{-y\} \sin x + 2\mu_* b_2 y. \quad (14)$$

The coefficients b_1 and b_2 will be determined below.

Using (12) and (14), we solve Eq. (2) with boundary conditions (7) and (10):

$$u = \exp\{-y\} \cos x (k - b_1 y), \quad (15)$$

$$v = \exp\{-y\} \sin x (A_2 + b_1 y) + b_2 y^2 + A_1, \quad (16)$$

where

$$A_1 = -\frac{a_4(c_d - c_0)L}{c_0(1 - c_0)2\pi d}, \quad (17)$$

$$A_2 = \frac{a_4 \alpha}{1 - c_0}, \quad (18)$$

$$k = \frac{-a_2 \alpha}{a_3 - 2a_1}. \quad (19)$$

Substituting (15) and (16) into (1), we obtain

$$b_1 = k + A_2, \quad b_2 = 0.$$

Hence,

$$u = \exp\{-y\} \cos x [k - (k + A_2)y], \quad (20)$$

$$v = \exp\{-y\} \sin x [A_2 + (k + A_2)y] + A_1 \quad (21)$$

In the approximation assumed, the longitudinal velocity is zero on the upper plate.

On the basis of (17) and (18) we introduce the stream function

$$\Psi = \exp\{-y\} \cos x [A_2 + (k + A_2)y] - A_1 x. \quad (22)$$

The flow has period 2π . Using (18) and (19), we obtain $k + A_2 > 0$. If $c_d < c_0$, then $A_1 > 0$; for $c_d > c_0$, we have $A_1 < 0$. In the first case there is a singularity at $x = 3\pi/2, 7\pi/2$; in the second case, at $x = \pi/2, 5\pi/2$. Solution of the characteristic equation shows that the singularity is a saddle point. Figure 1 shows streamlines corresponding to (22), for $k < 0$.

As in [1], ξ is of second order of smallness, and therefore $\sigma \approx -m\tau$.

If $c_0 = c_d$, then according to (17), we have $A_1 = 0$. In this case, both the longitudinal and transverse velocities equal zero on the upper plate.

Disregarding the effect of the transverse velocity component at the glass-wall boundary (i.e., replacing conditions (7) and (10) by the condition $v = 0$ for both plates), we obtain

$$u = k(1 - y) \exp\{-y\} \cos x,$$

$$v = ky \exp\{-y\} \sin x,$$

$$\Psi = ky \exp\{-y\} \cos x.$$

In this case the streamlines are closed curves with singularities of the "center" type, having coordinates $x = 0, \pi, 2\pi, \dots; y = 1$. These results agree with the results obtained in [1] for the flow of a one-component rarefied gas with sinusoidal temperature distribution at the wall.

Thus, taking account of the effect of the transverse velocity component at the plate-gas boundary substantially changes the nature of such flows.

NOTATION

$$\Delta = \partial^2 / \partial x^2 + \partial^2 / \partial y^2;$$

p and ρ

are the gas pressure and density;

T

is the gas temperature;

u and v

are the longitudinal and transverse velocity components;

μ

is the coefficient of viscosity of the gas;

D_{12}

is the binary diffusion coefficient;

R_1 and R_2

are the gas constants of the components;

c

is the concentration of component 1;

f

is the accommodation coefficient.

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